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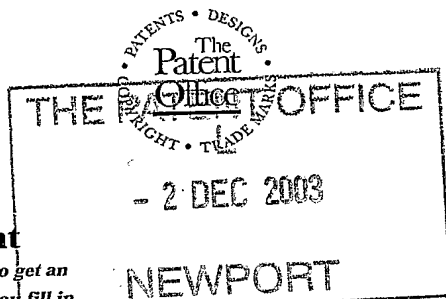
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P01/7700 0.00-0327863.7

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1. Your reference

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2. Patent application number

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0327863.7

3. Full name, address and postcode of the or of each applicant (underline all surnames)

Heriot-Watt University
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EH14 4AS

Patents ADP number (if you know it)

05532072001

If the applicant is a corporate body, give the country/state of its incorporation

UK

4. Title of the invention

Electrochemcial sensor

5. Name of your agent (if you have one)

"Address for service" in the United Kingdom to which all correspondence should be sent (including the postcode)

Kennedys Patent Agency Limited

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G1 2DT

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Country

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Date of filing
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Number of earlier application

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- a) any applicant named in part 3 is not an inventor, or
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Description 10

Claim(s)

Abstract

Drawing(s) 4 + 4

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Priority documents

Translations of priority documents

Statement of inventorship and right to grant of a patent (Patents Form 7/77)

Request for preliminary examination and search (Patents Form 9/77)

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Any other documents (please specify)

11. I/We request the grant of a patent on the basis of this application.

Signature Kennedy

Date

KENNEDYS

1 December 2003

12. Name and daytime telephone number of person to contact in the United Kingdom

Simon Black

Tel: 0141 226 6826

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1 Electrochemical sensor

2

3 The present invention relates to an electrochemical
4 sensor apparatus and method and, in particular to an
5 electrochemical sensor that can be used to measure scale,
6 such as mineral scale or other particulates, which
7 deposit on the surface of pipelines or process equipment.

8

9 Mineral scale formation is one of the major flow
10 assurance concerns in the chemical industry. The problem
11 of scale build up arises where a fluid is flowing through
12 a pipe or vessel and particulates precipitate out from
13 the fluid and deposit on the surfaces of fluid-carrying
14 equipment. This can cause a blockage to form and the
15 eventual failure of the equipment or disruption in the
16 flow of the fluid.

17

18 This problem is particularly apparent in the offshore oil
19 and gas industry. If the formation of scale or other
20 particulate masses goes uncontrolled, the operational
21 safety of the process or plant equipment can be
22 compromised through the failure of subsea safety and flow
23 control valves or other process equipment. If, for

1 example, a large mass of mineral scale forms in the riser
2 from an oil well, the mass of scale will cause the riser
3 to be blocked, consequently the flow of oil well fluids
4 will be impeded and the pressure will greatly increase,
5 thereby causing the riser to break.

6
7 In view of this problem, it is desirable to be able to
8 measure the amount of scale that has formed within a
9 conduit or vessel, and also to be able to estimate and
10 monitor the changes of the scaling potential of a fluid
11 to precipitate out scale or other particulates. A
12 measurement of the surface deposition on control surfaces
13 or changes of scaling tendency will alert the operator.
14 Hence, allows the operator of the well or chemical
15 process to treat the fluid in order to prevent scaling.

16
17 Current methods for monitoring the extent of surface
18 scaling and the scaling tendency in reservoirs or pipes
19 have limitations. They tend to involve measuring water
20 or other fluid samples, or to involve the measurement of
21 flow variables such as pressure. These methods do not
22 allow the operator to predict whether scaling will occur.
23 Scale detection often comes too late using this type of
24 monitoring, only after the decrease of the production. In
25 general, efforts to control the scaling problem have
26 concentrated upon strategies to mechanically or
27 chemically remove scale.

28
29 It is an object of the present invention to develop an
30 electrochemical sensor that allows the operator to
31 measure the extent of scale formation on a metal surface
32 and to assess the scaling tendency of a fluid.

33

1 In accordance with a first aspect of the present
2 invention, there is provided an electrochemical sensor
3 comprising:

4
5 an electrical cell having a working electrode;
6 fluid flow control means, the fluid flow control means
7 being positioned so as to release a fluid jet onto the
8 working electrode, the fluid jet having a predetermined
9 velocity defined by the Reynolds number of the fluid when
10 the fluid is in the fluid flow control means; and
11 electrical output measurement means
12 wherein control of the Reynolds number and measurement of
13 the electrical output from the electrical cell provide a
14 measure of the build-up of scale on the working
15 electrode.

16
17 Preferably, the electrochemical sensor of the present
18 invention is provided with means for measuring the
19 quantity of scale build up and/or the scaling tendency of
20 the fluid.

21
22 Preferably, the electrical output measurement means
23 measures the limiting current response of the electric
24 cell as a function of Reynolds Number.

25
26 Preferably, the electrical output measurement means
27 measures the limiting current from an electrochemical
28 tracer as a function of Reynolds number.

29
30 Preferably, the apparatus of the present invention
31 further comprises fluid sampling means for obtaining a
32 sample of a test fluid.

1 Preferably, the fluid sampling means contains fluid
2 isolation means for isolating the test fluid from a bulk
3 fluid.

4

5 Preferably, the test fluid isolation means is provided by
6 a container having at least one sealable valve which,
7 when opened, allows the test fluid to enter the sampling
8 means.

9

10 Preferably, the fluid flow control means comprises a flow
11 meter connected to a conduit from which said fluid jet is
12 expelled.

13

14 Preferably, the electrical cell further comprises a
15 counting electrode and a reference electrode.

16

17 In accordance with a second aspect of the present
18 invention, there is provided a method of measuring the
19 scaling potential of a test fluid, the method comprising
20 the steps of:
21 controlling the velocity of a fluid jet by control of the
22 Reynolds number of said fluid when said fluid is housed
23 in a fluid control means;
24 releasing the fluid jet from the fluid control means onto
25 a working electrode of an electrical cell; and
26 measuring the electrical output from the electrical cell
27 as a function of the Reynolds number of the jet fluid,
28 the working electrode being in contact with a sample of
29 the test fluid..

30

31 Preferably, the method comprises the further step of
32 isolating the test fluid from a flowing fluid prior to

1 measuring the electrical output from the electrical cell
2 as a function of the Reynolds number of the fluid.

3

4 Preferably, the test fluid is isolated by closing valves
5 arranged upstream and downstream of a predetermined
6 measuring location in a sample measuring means.

7

8 It has been found that isolation of a sample of the fluid
9 allows the Reynolds number of the analysing fluid to be
10 carefully controlled by the sensor device.

11

12 Preferably the fluid is isolated by removably attaching a
13 sampling conduit to a first conduit in which the bulk of
14 the fluid is situated, and by providing valves to isolate
15 the sampling conduit from the first conduit.

16

17 In accordance with a third aspect of the present
18 invention, there is provided a computer program for use
19 with apparatus of the first aspect of the present
20 invention, and with the method of the second aspect of
21 the present invention, in which analysis of the
22 electrical output and the Reynolds number provides
23 information on the quantity of scale build up and/or the
24 scaling tendency of the fluid.

25

26 The present invention will now be described by way of
27 example only, with reference to the accompanying
28 drawings, in which:

29

30 Figure 1 is a schematic diagram of an embodiment of the
31 apparatus of the present invention;

32

1 Figure 2 is a graph of the limiting current output of the
2 electrochemical cell, as measured against the square root
3 of the Reynolds number of the jet fluid;

4
5 Figure 3 is a schematic representation of the second
6 embodiment of the present invention, where the
7 electrochemical cell is positioned in a conduit,
8 removably connected to a riser; and

9
10 Figure 4 shows the limiting current correlation with
11 scaling index of the water. The correlation between the
12 supersaturation ratio and the electrochemical measurement
13 make it possible to measure the scaling tendency of the
14 water.

15
16 Figure 1 shows an electrochemical sensor setup comprising
17 an electrochemical cell rig 3, having the following
18 components. The electrical cell 3 comprises a working
19 electrode 21 position proximate and normal to the nozzle
20 9 through which a fluid jet (also known as an impinging
21 jet) exits from the nozzle 9. In addition, the cell rig
22 18 provides support for a reference electrode 19 and a
23 counting electrode 23 made of platinum, in this example.

24
25
26 The fluid control means consists of a pump 15 positioned
27 downstream of a needle valve 13 which is used to control
28 the flow level of the impinging jet fluid. A flow meter
29 7 is used to measure the amount of flow of the impinging
30 jet fluid so as to allow calculation of the Reynolds
31 number of the jet fluid. A nozzle 9 provides the means
32 by which the impinging jet fluid exits the fluid control
33 means 5 and contacts the working electrode 21. In this

1 example, a solution tank is provided for storage and
2 circulation of the impinging jet fluid.

3 Figure 2 is a graph of the limiting current i_L measured
4 against the square root of Reynolds number ($Re^{1/2}$). The
5 graph 41 shows three curves. The first curve illustrates
6 a situation in which no scale has been deposited upon the
7 working electrode from the test fluid. Curve 45
8 illustrates the situation on an unscaled sensor. Curves
9 46, 47 and 48 illustrate the response from the sensor
10 with 22%, 39% and 46% of scale coverage respectively
11 after immersion for 1, 9 and 24 hours in a scaling
12 solution. These schematic representations clearly show
13 the difference in the limiting current over the same
14 range of Reynolds number, where the level of scaling in
15 the sample is different.

Immersion Time,Hrs	%Scale Coverage
1	22
9	39
24	46

17

18 Table 1 shows the resultant scale coverage for different
19 immersion times.

20 In use, the fluid control means or impinging jet system 5
21 is submerged in a fluid sample, and is used to control
22 the hydrodynamic regime at the surface of the working
23 electrode 21. Through analysis of the kinetics of the
24 oxygen reduction reaction on the sensor surface, the
25 extent of scaling and the scaling tendency of the fluid
26 can be determined. In this example the test fluid is
27 water.

28

1 The potential of the electrochemical sensor 1 is applied
2 to -0.8 volts (with respect to a silver/silver chloride
3 system) when measurements are started. The impinging jet
4 system is then controlled through a range of Reynolds
5 numbers, and the limiting current response is measured as
6 a function of the Reynolds number. Measuring the
7 relationship between these two variables, enables the
8 scaling information to be obtained. In this way, the
9 amount of scale and the scaling tendency of the test
10 fluid can be determined.

11

12

13 Figure 4 shows the limiting current correlation with
14 scaling index of the water (brine) for 6000s. The
15 correlation between the supersaturation ratio and the
16 electrochemical measurement make it possible to measure
17 the scaling tendency of the water.

18

19 Figure 3 shows a second embodiment of the present
20 invention, in which the cell rig is installed in the
21 bypass system and the Reynolds number is controlled
22 through valves located in the inlet and outlet of the
23 bypass.

24 As shown in Figure 3, the bulk fluid 33 flows down
25 conduit 31 and a sample (the test fluid) of the bulk
26 fluid 33 is tapped from the bulk fluid conduit 31 to
27 measurement conduit or bypass system 35. Once the sample
28 of the bulk fluid has been tapped, valves 37 and 39 are
29 closed to enable measurements of the extent of scale or
30 the scaling tendency of the sample to be taken. The
31 impinging jet is directed onto the sample and the fluid
32 surrounding the sensor is essentially static.

1

2 The ability to operate the electrochemical sensor of the
3 present invention in situ allows the scaling tendency and
4 scale coverage to be monitored as the pressure,
5 temperature, water chemistry and other environmental
6 conditions change. By locating the apparatus of the
7 present invention within the precise zone of interest
8 within a pipeline, the present invention can monitor the
9 scaling tendency and scale coverage from individual
10 branches of a pipe in, for example, a horizontal well
11 which goes into the main pipeline. Information feedback
12 from the well can provide an early indication of scaling
13 potential problems. Hence, the present invention enables
14 the operator to manage and selectively control individual
15 wells and to inject the correct amount of scale inhibitor
16 in these wells.

17

18 Further advantageously, the present invention can detect
19 small amounts of scale and can rapidly (within a matter
20 of 30 minutes or so) determine the scaling tendency of
21 the sample. As a consequence, the operator of the
22 conduit, whether it be a riser from an oil well, a subsea
23 pipeline, a pipe in a desalination plant, or otherwise,
24 can quickly determine the scaling tendency in these
25 positions and can anticipate problems associated with the
26 build up of scale.

27

28 In use, the apparatus of the present invention will be
29 connected to an operator terminal by means of a suitable
30 telemetry system. This will allow data to be collected

1 frequently by the operator using a communications
2 protocol. Real-time data from the oil well or other
3 location will be sent to a PC based surface system that
4 monitors this location. In addition, multiple systems
5 can be used at varying locations in a pipeline system or
6 well or the like, and all of these individual systems can
7 feed data back to a single PC for analysis by the
8 operator, who may then use this data to determine it is
9 necessary to add chemical scale inhibitors to that
10 location, or to otherwise remove or limit the scale
11 measured at that location.

12

13 The present invention has a number of advantages over the
14 known prior art. In particular, the present invention
15 allows early measurement of scale or other particulates,
16 and provides a means by which the scaling tendency of the
17 fluid in question can be measured. Measurement of the
18 scaling tendency, as well as the bulk amount of scale,
19 allows the operator to predict the amount of inhibitor
20 that should be used, and also to predict when in the
21 future this inhibitor should be applied.

22

23 Improvements and modifications may be incorporated
24 herein, without deviating from the scope of the
25 invention.

26

1/4

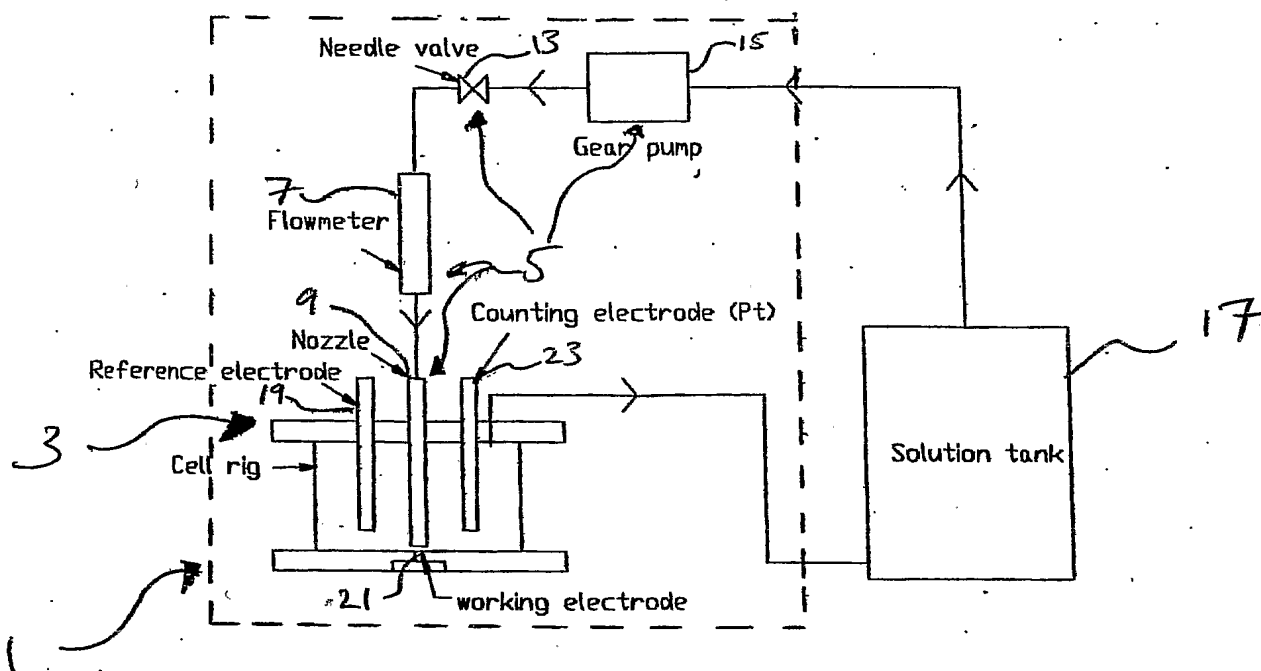


FIGURE 1



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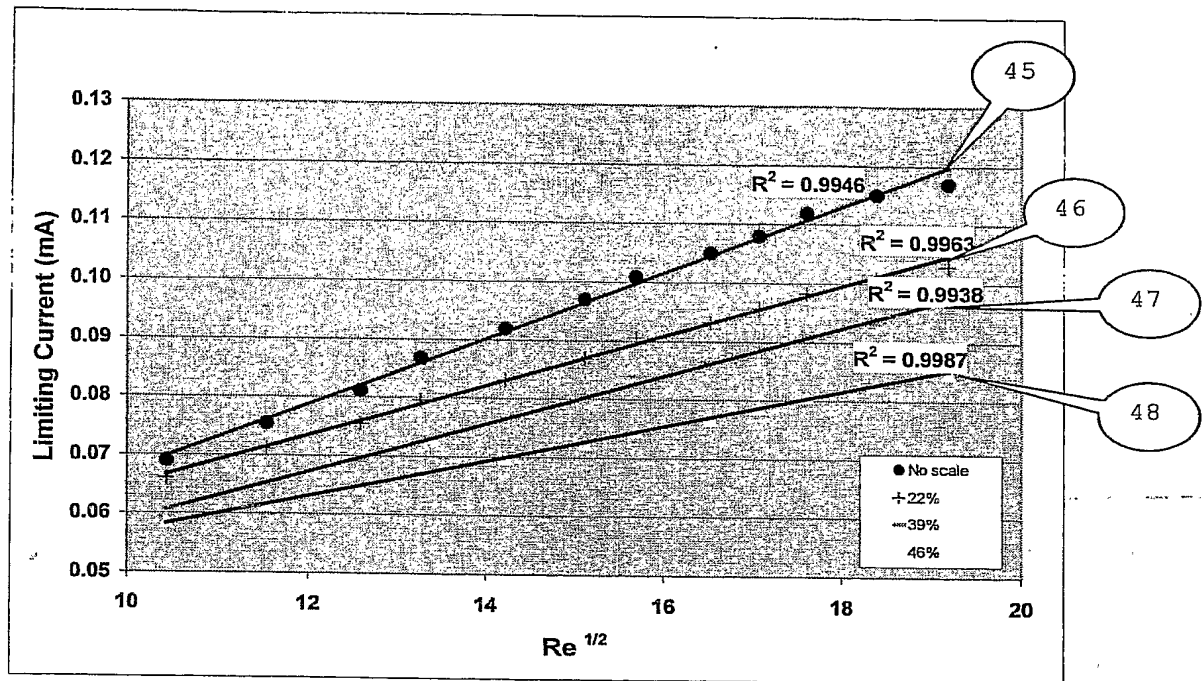


Figure 2



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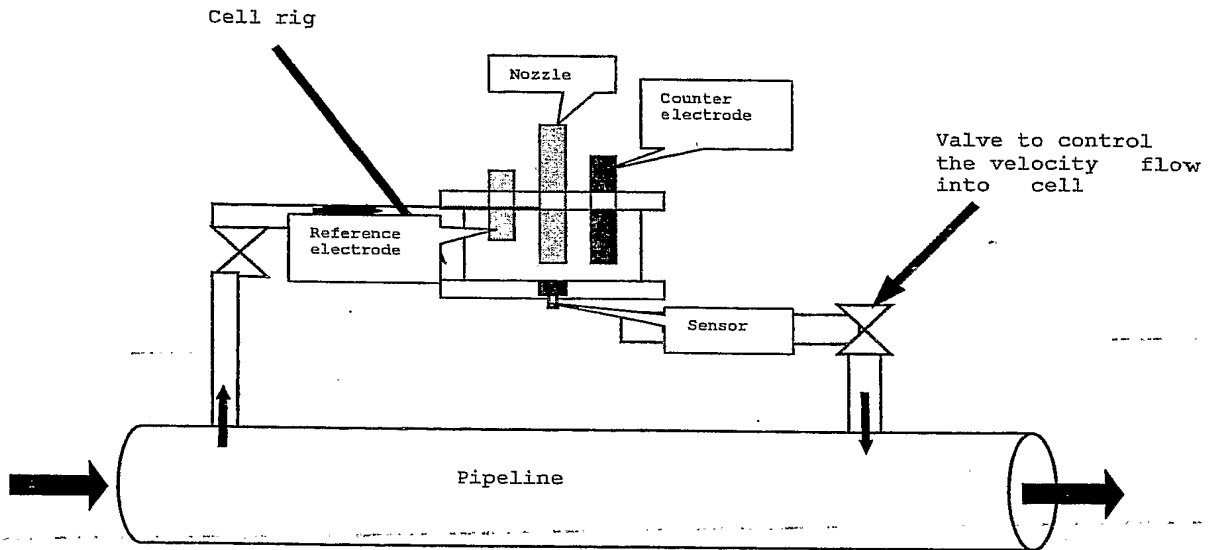


Figure 3



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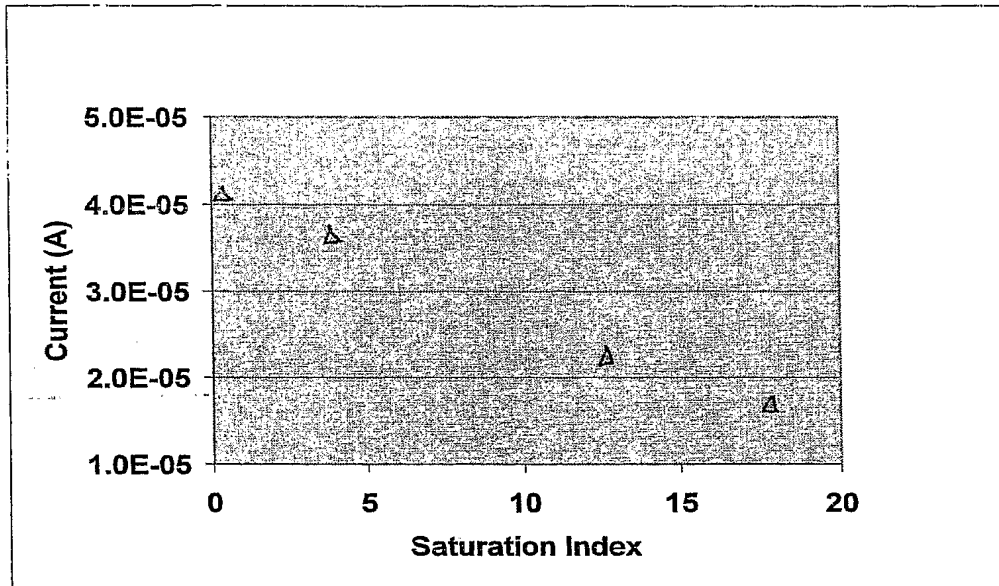


Figure 4

